

Selective Hydrogenation of Crotonaldehyde to Crotyl Alcohol
on Ag-MnO₂/Al₂O₃·5AlPO₄ Catalysts

Yoshinori NAGASE,* Hideaki MURAMATU, and Takuzi SATO

Department of Industrial Chemistry, Faculty of Engineering,
Ibaraki University, Hitachi, Ibaraki 316

The activity and selectivity of Ag-MnO₂/Al₂O₃·5AlPO₄ catalysts for the hydrogenation of crotonaldehyde to crotyl alcohol have been investigated in liquid phase. When MnO₂ was added to the catalyst, the activity and selectivity for the reaction were remarkably improved to give the conversion of 100 mol% and the selectivity of 69.5%.

α - β -Unsaturated aldehyde which has both C=C and C=O double bonds is preferentially hydrogenated to saturated aldehyde in most case, followed by the successively hydrogenation to saturated alcohol. On the other hand, unsaturated alcohol formed with the hydrogenation of unsaturated aldehyde undergoes isomerization to saturated aldehyde, and also a partial dehydrogenation, accordingly it is difficult to obtain a high yield of the corresponding unsaturated alcohol by means of the selective hydrogenation of unsaturated aldehyde. A few catalyst suitable for giving a high yield of unsaturated alcohol from the above reaction have been reported up to now. For example, mild hydrogenation catalysts such as noble metal, 1) transition metal, 2) Raney-type metal³⁾ and catalysts with Cd⁴⁾ have been reported to show a high activity and selectivity for the above reaction. Rylander et al. hydrogenated crotonaldehyde to crotyl alcohol in ethanol over platinum-zinc-iron catalyst in 1963.⁵⁾ Yada et al. reported a yield of 50 mol% of crotyl alcohol at 225-250 °C from crotonaldehyde at 80% conversion.⁶⁾ Vanderspurt hydrogenated acrolein to obtain a high yield of allyl alcohol over Raney-type silver-cadmium catalyst.⁷⁾ Recently, Noller et al. hydrogenated crotonaldehyde to obtain 54 mol% crotyl alcohol of the usual maximum yields over Cu-Ni/Al₂O₃ catalyst in a flow system at 80 °C.⁸⁾

It was recognized in this study that the $\text{Ag-MnO}_2/\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ catalyst for the selective hydrogenation of crotonaldehyde showed a high activity with a yield of 69.5 mol% of crotyl alcohol. This catalyst is superior to the former cases.

The catalyst was prepared by the coprecipitation and impregnation methods according to the following procedure ; 25% ammonium aqueous solution was added to a mixed solution of aluminium nitrate and phosphoric acid at pH=8. The gel precipitates thus obtained were successively impregnated with silver nitrate solution for 15 h, and then vaporized in water bath at 60 °C for 8 h. These materials were dried in air oven at 120 °C for 20 h, and thereafter calcined at 500 °C for 10 h in an electric furnace (Ag-AAP). As the next procedure, Ag-AAP was impregnated with a fixed magnesium nitrate solution. The procedures of vaporizing, drying, and calcinating described above were repeated respectively. As the final catalyst containing of 20 wt% Ag, $\text{Ag-MnO}_2/\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ was obtained.

The reaction was carried out by using powder catalyst less than 40 mesh particles. A 300 ml autoclave was employed for carrying out the reaction. A mixture of 10 ml crotonaldehyde and 90 ml hexane was introduced into the autoclave with catalyst of 1.0 g. The reaction was performed at 100-200 °C for 30-180 min under an initial hydrogen pressure of 50 atm. The reaction products were analyzed by gas chromatography with thermal conductivity detector. Column ; Carbowax 20 M (0.6 cm x 2 m) and Reoplex 400 (0.6 cm x 1 m), 80-100 mesh.

The results are summarized in Table 1 and Table 2.

Table 1. Activity and selectivity for the hydrogenation of crotonaldehyde on $\text{Ag-MnO}_2/\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ catalyst ^{a)}

Catalyst	Reaction temp/ °C	Composition product (mol%)				Conversion	Selectivity
		Crotyl alcohol	Butyr-aldehyde	Butyl alcohol	Rest		
Ag / AAP	130	28.9	26.2	4.1	0	59.8	48.8
	150	38.4	30.2	19.5	0	84.6	41.2
	170	23.0	33.7	21.1	6.5	84.5	27.5
$\text{Ag-MnO}_2/\text{AAP}$ (Mn/Ag = 3)	150	68.5	12.8	16.6	0	97.9	70.0
	170	60.2	3.8	32.3	3.0	99.3	60.6
$\text{Ag-MnO}_2/\text{AAP}$ (Mn/Ag = 5)	150	69.5	9.2	19.0	2.3	100.0	69.5
	170	63.5	10.2	21.0	3.7	98.3	64.6

a) Feed ; crotonaldehyde 10 ml, hexane 90 ml, initial hydrogen pressure 50 atm, reaction time 2 h, catalyst 1.0 g, Mn/Ag ; atomic ratio, AAP ; $\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$.

As shown in Table 1, the activity and selectivity for the hydrogenation of crotonaldehyde were examined by using $\text{Ag-Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ catalyst. The conversion of crotonaldehyde was increased with an increase of reaction temperature and the selectivity was decreased. On the other hand, the results of the hydrogenation of acrolein on $\text{Ag-Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ catalyst is shown in Table 2.

Table 2. Activity and selectivity for the hydrogenation of acrolein on $\text{Ag-MnO}_2/\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ catalyst ^{a)}

Catalyst	Reaction temp / °C	Composition product (mol%)				Conversion	Selectivity
		Allyl alcohol	Propion aldehyde	Propanol	Rest		
Ag / AAP	130	14.0	21.0	0	0	35.5	40.0
	150	30.2	44.7	0	0	74.9	40.3
	170	37.4	48.4	7.8	3.6	97.3	38.5
Ag-MnO ₂ /AAP (Mn/Ag = 3)	150	49.6	22.2	18.7	9.3	99.9	49.7
	170	49.5	9.3	35.2	5.1	99.1	49.9
Ag-MnO ₂ /AAP (Mn/Ag = 5)	150	52.9	17.9	19.1	9.8	99.6	53.1
	170	49.7	12.3	30.3	5.9	98.1	50.6

a) Feed ; acrolein 10 ml, hexane 90 ml, initial hydrogen pressure 50 atm, reaction time 2 h, catalyst 1.0 g, Mn/Ag ; atomic ratio, AAP ; $\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$.

As shown in Table 2, the reaction had a high conversion, but the selectivity as low as 40% independently of conversion. However, as these results were unsatisfactory in the selectivity of the reaction, catalyst containing of other metal as researched. Effect of activity and selectivity for the hydrogenation of crotonaldehyde on catalyst containing of Mn added to $\text{Ag-Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ is shown in Table 1 and Fig. 1. As observed in Table 1 and Table 2, above both reactions on catalysts containing of MnO₂ had a high conversion and selectivity. As shown in Fig. 1, Mn addition to the catalyst (Mn/Ag 2-5 atomic ratio) was allowed to increase conversion and selectivity. When MnO₂ (Mn/Ag = 5 atomic ratio) was added to Ag-AAP catalyst, a yield of crotyl alcohol was improved from 34.9 mol% yields of Ag-AAP catalyst to 69.5 mol% at 150 °C. From another preliminary experiments, it was thought that MnO₂ addition to the catalyst promoted the hydrogenation of the C=O group of unsaturated aldehyde, and moreover gave a high yield due to inhibit a partial dehydrogenation of unsaturated alcohol.

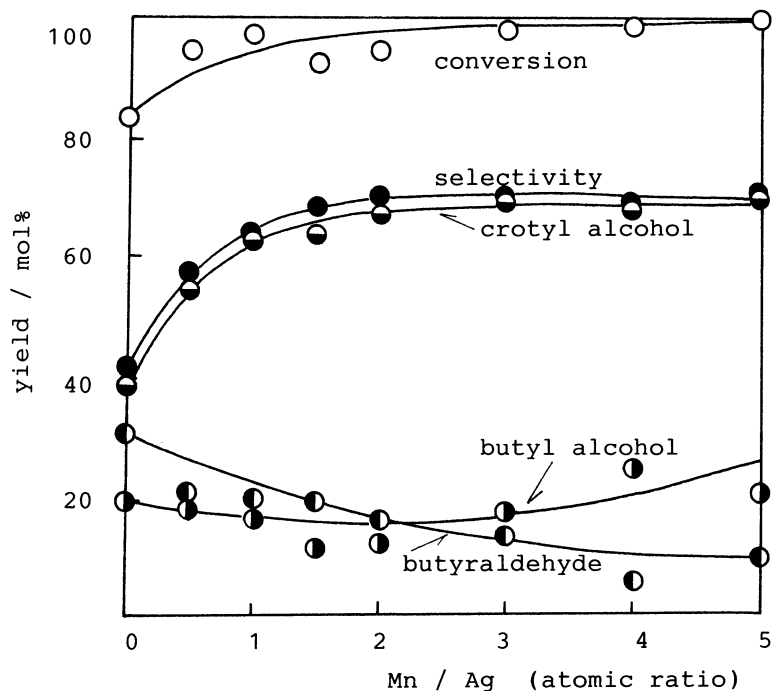


Fig. 1. Effect of activity and selectivity for the hydrogenation of crotonaldehyde on catalyst of Mn added to $\text{Ag-Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$

It was found in this study that $\text{Ag-MnO}_2/\text{Al}_2\text{O}_3 \cdot 5\text{AlPO}_4$ catalyst had a high conversion of 100 mol% and selectivity of 69.5% for the above reaction of crotonaldehyde at 150 °C. This result is superior to the usual maximum yields of crotyl alcohol 54 mol%.

References

- 1) H.S. Broadbent, G.C. Campbell, W.B. Bartley, and J.H. Johnsons, *J. Org. Chem.*, **24**, 1847 (1959).
- 2) L.J. Richard, M.H. Delbelt, and S.M. Darrel, U.S. Patent 4292452 (1981).
- 3) L.Kh. Freidlin, A.S. Sultanov, and M.F. Abidova, *Izv. Akad. Nauk. SSSR, Otdel. Khim. Nauk*, **1958**, 378.
- 4) T.H. Vanderspurt, U.S. Patent 4020116 (1977).
- 5) P.N. Rylander, N.G. Himelstein, and M. Kilroy, *Engelhard Ind. Technol. Bull.*, **4**, 49 (1963).
- 6) S. Yada, T. Yamauchi, and S. Kudo, *Shokubai*, **5**, 1 (1963).
- 7) T.H. Vanderspurt, Celanese Corp. U.S. Patent 4127508 (1978).
- 8) H. Noller and W.M. Lin, *J. Catal.*, **85**, 25 (1984).

(Received July 2, 1988)